Hydrogen Winter School – University of Birmingham





#### Artur J Majewski



### AmmoGen project



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#### Ammonia saved the world once







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## Ammonia facts



2<sup>nd</sup> most produced chemical worldwide

50% of world population rely on ammonia-based fertilisers for food

400 million tons of annual carbon emissions from ammonia manufacture

2% of global energy consumption is ammonia manufacture

3 kWh/L energy density – highest among zero-carbon fuels









#### Haber-Bosch process



Fritz Haber

The Haber-Bosch process takes nitrogen from the air and converts it to ammonia.

it makes possible to produce **synthetic fertilisers** and produce sufficient food for the growing population



Carl Bosch

#### But

It is also a key raw material in the production of high explosives



## History of ammonia synthesis

Solving the problem earned Haber and Bosch two **Nobel Prizes** in chemistry: Haber in 1918, Bosch in 1931.

- **1774** Joseph Priestley, isolated gaseous ammonia.
- **1785** ammonia composition determined Claude Louis Berthollet
- **1898** Adolph Frank and Nikodem Caro found that N<sub>2</sub> could be fixed by calcium carbide to form calcium cyanamide, which could then be hydrolyzed with water to form ammonia:
- **1906-8** Haber (with R. Rossignol), decided to use **high-pressure process** for ammonia synthesis
- 1909 they patented this process with yield 15% ammonia, at 175 atmospheres 550°C, over an osmium and uranium catalyst
  1913 Badische Anilin und Soda Fabrik (BASF) engineer Carl Bosch started scaling up the process











# Challenges in scaling up

- Source of hydrogen (water-gas + Linde-Frank-Caro process = H<sub>2</sub>)
- Catalyst mixed catalyst based on iron oxide - still in use today
- Pressure vessels







The first plant to use the Haber-Bosch process at industrial scale by BASF in 1913.

#### BASF designed :

- externally-heated contact tube reactor (But the material became brittle, and the tubes burst).
- the first lined reaction chamber a pressure-bearing steel jacket thinly lined with a soft steel.
- heating the reactor from the inside
- compressors, monitoring instruments to measure temperature, the intensity of the gas stream and the composition of the gas in the reaction chamber

Over 100 years on and nothing much has changed, and the process is still used around the world.





### **Global Hydrogen Markets**



### **Ammonia production**

Oil O Fossil with CCU O Gas O Coal



source: IEA









 $\mathrm{N}_2 + 3\,\mathrm{H}_2 \rightleftharpoons 2\,\mathrm{NH}_3 \qquad \Delta H^\circ = -92.28~\mathrm{kJ}~(\Delta H^\circ_{298\mathrm{K}} = -46.14~\mathrm{kJ/mol})$ 

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 $\mathrm{CH}_{4(\mathrm{g})} + \mathrm{H}_2\mathrm{O}_{(\mathrm{g})} \longrightarrow \mathrm{CO}_{(\mathrm{g})} + 3\,\mathrm{H}_{2(\mathrm{g})} \qquad \Delta H = +206\;\mathrm{kJ/mol}$ 





Production of the synthesis mixture







 $\mathrm{N}_2 + 3\,\mathrm{H}_2 \rightleftharpoons 2\,\mathrm{NH}_3 \qquad \Delta H^\circ = -92.28~\mathrm{kJ}~(\Delta H^\circ_{298\mathrm{K}} = -46.14~\mathrm{kJ/mol})$ 



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### Haber-Bosch plant





 $\mathrm{CH}_{4(\mathrm{g})} + \mathrm{H}_2\mathrm{O}_{(\mathrm{g})} \longrightarrow \mathrm{CO}_{(\mathrm{g})} + 3\,\mathrm{H}_{2(\mathrm{g})} \qquad \Delta H = +206\;\mathrm{kJ/mol}$ 

$$\begin{split} 2\operatorname{CH}_{4(\mathrm{g})} + \mathrm{O}_{2(\mathrm{g})} &\longrightarrow 2\operatorname{CO}_{(\mathrm{g})} + 4\operatorname{H}_{2(\mathrm{g})} \qquad \Delta H = -71 \text{ kJ/mol} \\ & \mathrm{CO}_{(\mathrm{g})} + \mathrm{H}_2\mathrm{O}(\mathrm{g}) \longrightarrow \mathrm{CO}_{2(\mathrm{g})} + \mathrm{H}_{2(\mathrm{g})} \qquad \Delta H = -41 \text{ kJ/mol} \\ & \mathrm{N}_2 + 3\operatorname{H}_2 \rightleftharpoons 2\operatorname{NH}_3 \qquad \Delta H^\circ = -92.28 \text{ kJ} \left(\Delta H_{298\mathrm{K}}^\circ = -46.14 \text{ kJ/mol}\right) \quad 15 \end{split}$$





### **Ammonia Synthesis & Cracking**

Haber Bosch:

Fe-catalyst, 500°C, 150-200 bar



1.4 MWh/to total energy input



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### Steam Reforming (Diagram)

Ammonia Cracking (Diagram)



 $H_2$ 





#### Ammonia cracking catalyst

- Typically 700 950°C, Ni-based catalyst,
- 450 500°C, Ru/Co-based catalyst
- Pressure ~80 bar







#### volumetric energy density of fuels



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- Toxicity
- Corrosive to some alloys containing copper and nickel and to some plastics
- Difficult to ignite and doesn't sustain combustion well
- When burned at high temperatures, ammonia produces nitrogen dioxide and nitrous oxide
- Caustic in aqueous solution (high pH value, use as bleach), tanker spill could have considerable negative impact on sea life
- Energy intensive, 'green' ammonia will need to look carefully at the energy inputs







ammonia to hydrogen conversion project

**Introduction to the AmmoGen Project** 



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1 use of low-cost green energy, e.g. Middle East, North Africa, Australia etc. to produce hydrogen



transport hydrogen to UK & Europe



feed low(er)-cost hydrogen into the energy system

Turning hydrogen into ammonia and back again allows for considerably more compact transport and thus lower cost of overall operations.



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operate and Project manage the management facility FEQUANS Gemserv A **Talan**<sup>\*</sup>Company provide the host location supply ammonia for the project TYSELEY ENERGY PARK funding for Ammogen cracking technology H2 SITE Dissemination, supply of ammonia liquid UNIVERSITY<sup>OF</sup> BIRMINGHAM ammonia storage **YARA** 

LOS . Department for **Energy Security** & Net Zero

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#### Research & Demonstration Questions

- what are the real-world issues around using ammonia for H<sub>2</sub> transport?
   w.r.t.
- energy efficiency
- economic viability
- safety





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#### The Tyseley Energy Park – project concept













July 2023 construction starts Q3 & 4 2023

building & commissioning, test operation

## **2024** full operation

12/2024

#### decommissioning

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## UNIVERSITY<sup>OF</sup> BIRMINGHAM Ammonia drum decant







#### **Ammonia vaporiser**



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#### Thank you



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